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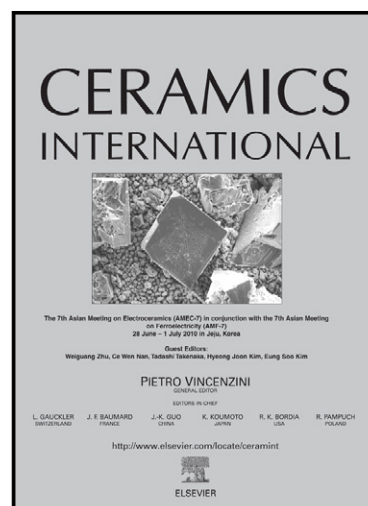
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Tailoring the microstructure of porous MgO supports for asymmetric oxygen separation membranes: Optimization of thermoplastic feedstock systems

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Abstract

Porous magnesium oxide (MgO) structures were prepared by thermoplastic processing for use as supports in asymmetric thin film oxygen transport membranes (OTMs). The open porosity, pore size distribution, and resulting gas permeability of the MgO structures were measured for different feedstock compositions and sintering temperatures. For a composition with 19 vol.% graphite as a pore-former, sintering temperatures of 1300 °C and 1400 °C, resulted in support porosities of 36% and 26%, respectively, and gas permeabilities of $1.4 \times 10^{-16} \text{ m}^2$ and $3.1 \times 10^{-16} \text{ m}^2$, respectively. Electron microscopy showed that the unexpected increase in gas permeability at temperatures above 1300 °C was a result of the growth of macro-pores and the opening of bottle-neck pores which resulted in improved pore connectivity. Mercury intrusion porosimetry experiments confirmed an increase in average pore size for samples sintered above 1300 °C, despite a significant decrease in total porosity.

Keywords

Oxygen transport membranes (OTM), magnesium oxide, thermoplastic feedstock, porous support, microstructure.

1. Introduction

Inorganic oxygen transport membranes (OTM) are of interest for high purity oxygen production and for integration into membrane reactors where high temperature oxygen is required [1]. Pure oxygen is used as a reactant/component in many industrial processes. Combustion of coal using oxygen instead of air removes nitrogen from the flue gas and makes subsequent CO₂ capture and sequestration significantly cheaper and more efficient. OTM technology has the potential to improve the process efficiency of a number of systems e.g. syngas production from methane [2–4]. In large-scale industrial syngas production, reactors operate in the temperature range of 700–1050 °C with a pressure between 2–4 MPa to achieve significant conversion efficiencies, and have very reducing atmospheres containing aggressive gases such as CO, CO₂ and H₂S. Hence, the ceramic oxygen membrane materials and their auxiliary parts have to be both chemically and structurally stable in order to withstand these harsh conditions for long periods of time. Dense mixed oxide ion- and electron-conducting (MIEC) ceramics based on Ce_{0.9}Gd_{0.1}O_{1.95-δ} (CGO10) are promising materials for this application and have recently demonstrated high oxygen fluxes of 16 Nml min⁻¹ cm⁻² at 900 °C under syngas production conditions [5], using a 30 μm planar CGO10 membrane supported on a Ni-YSZ support typically used for solid oxide fuel cells [6,7].

There have been significant efforts devoted to fabricating strong and highly-permeable porous support materials for oxygen transport membranes. Both planar and tubular configurations have been investigated along with various methods for fabricating these structures [8–12] in order to achieve high quality components. Thermoplastic processing [13] followed by extrusion is a good method for producing tubular structures, thin walled parts with a thickness below 1 mm and with close dimensional tolerances can be achieved [14]. Also, it is possible to recycle the feedstock from defective parts and reshape them. Using thermoplastic masses instead of water-based extrusion is advantageous as abrasion of the processing equipment (i.e extruder, chamber, and die head parts) is significantly reduced due to the high polymer content.

A support material for the use in asymmetric oxygen transport membranes should have a low cost, high thermal and chemical stability in the harsh operating environment, and good mechanical properties at elevated temperatures. MgO satisfies these requirements [15,16] and is also non-toxic (unlike previously-

reported perovskite and ceria-based materials) and is hence considered a good candidate for this application. MgO has relatively high thermal expansion coefficient (TEC) than other potential supports material such as YSZ or alumina[17]. However, the TEC of MgO is closer to the values for perovskites or ceria-based composites and it can be easily integrated with these membrane materials in order to prepare multi-layered structures without failures during processing as a result of expansion mismatches[18].

In addition, other factors relating to the processing, final microstructure, and use of the porous support need to be fulfilled:

a) A total open porosity of 35% to 40% after sintering to achieve sufficient gas permeation (at a support thickness of 0.5 to 1 mm).

b) For co-sintering of the support and the membrane layer it is important that the support layer has a similar sintering activity to the membrane layer to avoid cracking and defect formation during processing. This can be achieved by tailoring the particle size distribution of the raw ceramic powders.

c) For the final application, a membrane layer and thin catalytic layers (with thicknesses between 10 to 50 μm) need to be deposited on the MgO support by dip-coating, a thermoplastic coating process or infiltration and the support needs to be compatible with these processing steps (not discussed in detail in this paper).

In this study we describe the preparation and characterization of porous magnesium oxide supports made by thermoplastic processing. The thermoplastic feedstock composition and sintering conditions were varied to investigate their effects on the microstructure and gas permeability of the final porous structure. The processing conditions were further optimized with respect to co-sintering of the MgO with a ceria-based membrane layer.

2. Experimental

2.1 Raw materials

MgO powder (Product # 12R-0801, Inframat Advanced Materials, USA) was used for the preparation of the porous support along with a graphite powder (V-UF1 99.9, Graphit Kropfmühl AG, Germany) as a pore

former. The raw MgO powder was calcined at 1000 °C to reduce the surface area of the powder. Then the powder was coated with stearic acid dispersed in 1-propanol and mixed for 24 h using a ball mill before drying at 90 °C. This stearic acid coating reduced the tendency of the fine MgO raw powder to adsorb water and agglomerate, and improved powder handling (e.g. significantly reduced dust formation during the kneading process). J. Heiber et al. also showed that feedstock properties could be improved using pre-coated powders [19]. Measurements of the particle size distribution (PSD) were undertaken using a particle size analyzer (LS 13320, Beckman coulter, Inc, USA). BET surface areas of the powders were determined using an Autosorb-1 analyzer (Quantachrome Instruments, USA).

2.2 Feedstock preparation

In this study, the term “feedstock” refers to the mixture of thermoplastic and ceramic compounds used to prepare warm-pressed planar structures or extruded tubes. Previous studies [13] have shown that thermoplastic compositions designed for injection molding or thermoplastic extrusion can be shaped by warm pressing and give similar microstructures to extruded samples (when the process was carefully controlled). Warm-pressed samples were used here to investigate the microstructural and permeation properties as they are a simple geometry suitable for most of the characterization methods and only a small amount of feedstock was required (unlike extrusion; the proposed method for preparing OTMs in the future).

Feedstocks of MgO were prepared from MgO powder, graphite, a thermoplastic binder (Elvax 250, Du Pont; USA), paraffin wax (Sigma-Aldrich, USA) as a plasticizer, and stearic acid (Sigma-Aldrich, USA) as a dispersant. This system was developed for injection molding by Trunec et al. [20] and later also applied for thermoplastic extrusion. A Plastograph N50 (Brabender, Germany) was used to prepare the thermoplastic feedstocks with an operating temperature of 100 °C. The compositions of the prepared feedstocks are summarized in Table 1.

Table 1 about here

2.3 Preparation of porous MgO samples

The various feedstocks with different composition were warm-pressed into rectangular planar structures (35 mm x 50 mm) with a thickness of 1-2 mm using a uniaxial press (Model TP600, Fortune). A

load of 100 kN was applied for 2 min at 100 °C. After warm pressing the samples were heat treated (“debindered”) to remove the organic components and then sintered. These samples were used for thermogravimetry, dilatometry, and porosimetry experiments. The feedstock composition which was considered to have an optimized microstructure (MPG) was also extruded into tubes (14 mm outer diameter and 1 mm wall thickness) using a Brabender extruder 19/20DN in order to validate that the warm pressing and extrusion of an identical feedstock did indeed produce MgO components with the same properties. The ability to achieve identical properties via different processing will of course depend on the type of binder system, pore former, and plasticizer used.

For the preliminary studies on feedstock development, all samples were warm-pressed and sintered at 1275 °C for 2 h with a heating rate of 30 °C/h. Additionally, the warm-pressed feedstocks were sintered at various temperatures between 1250 °C and 1400 °C in order to investigate the influence of the sintering temperature on the final properties.

2.4 Characterization of the porous MgO samples

The properties of the different MgO feedstock compositions were characterized by dilatometry, density measurements, mercury intrusion porosimetry, permeability measurements, and electron microscopy, as described in detail in this section.

The geometrical densities of the warm-pressed samples were measured. The packing density of green (as-prepared) samples was calculated from the ratio between the measured green density and the expected green density (calculated by the density and volume fraction of each feedstock component).

The microstructure of the samples was studied using scanning electron microscopy (SEM) (SUPRA35, Carl Zeiss, Germany). The samples for the microstructural characterization were prepared using lap polishing with decreasing coarseness of sandpaper/polishing solution, where the last stage of polishing used 0.25 µm diamond paste.

A differential contact dilatometer (DIL 402 CD, Netzsch GmbH, Germany) was used to measure the sintering behavior and to characterize the densification behavior of the thermoplastic feedstocks. The samples were pellets cut from the warm-pressed sheets of MgO. An Al₂O₃ reference sample was measured

simultaneously with the sample. The heating rate was 3 °C min⁻¹ to a final temperature of 1450 °C. All experiments were conducted in air with a flow rate of 100 ml min⁻¹.

Porosimetry measurements were conducted using a mercury intrusion porosimeter (AutoPore IV 9510, Micromeritics, Norcross/GA, USA).

Gas permeation measurements were carried out using a system developed in-house. The setup consisted of a gas supply unit, a testing chamber and a unit for measuring the flow of the gas that permeates through the sample. A pressure difference across the sample was created using an electro-pneumatic pressure controller (Tescom, ER3000, USA). The flow of permeated gas was measured using an electronic flow meter (Agilent 5314, USA). The measurements were made with a pressure difference of 200 kPa at room temperature and with nitrogen as the permeate gas. Nitrogen was used for the experiments as it is safe and easy to work with and considered to give similar permeation data to oxygen (the gas of interest for OTM).

MgO supports (MPG) sintered at 1250 °C, 1300 °C, 1350 °C, and 1400 °C were used for the gas permeation measurements in order to quantify the gas permeability using the Darcy equation:

$$j = -k/\mu \cdot \nabla P \quad (1)$$

where, k is the permeability (m²), j is the flux (m³/ m² .s), μ is the viscosity of the gas (Pa.s), and ∇P is the pressure gradient (pressure (Pa)/sample thickness (m)).

Fig. 1 shows that the microstructure of MgO supports prepared by warm pressing is comparable to that of an extruded tube made from the same feedstock MPG (sintering at 1300 °C for 2 h). Additionally, the properties of the warm-pressed and extruded parts were identical with respect to gas permeability ($1.3 \pm 0.1 \times 10^{-16}$ m²) and total open porosity ($36 \pm 1\%$), validating that the warm pressing method is suitable for preparing samples for studying feedstock compositions for thermoplastic extrusion, as observed previously [13].

Fig. 1 about here

3. Result and discussion

3.1 Raw materials and feedstock composition

Table 2 summarizes the results of BET gas adsorption, particle size distribution (PSD), powder density and agglomeration factor (AF) for the raw powders. The agglomeration factor (AF) was calculated from the following equation[21].

$$AF = S_{BET} \times d_{50} \times \rho / 6 \quad (2)$$

where, S_{BET} , d_{50} and ρ are specific surface area, median particle size, and powder density respectively.

The uncalcined MgO powder had a very large surface area, (78 m²/g as measured by BET), and consisted of extremely fine (nanometric) primary particles that could not be fully de-agglomerated by kneading or dispersion in stearic acid, as indicated by a very high agglomeration factor of 140. Calcining the MgO powder at 1000 °C for 10 h reduced the specific surface area by almost a factor of eight and the agglomeration factor by a factor of 14. Further de-agglomeration of the pre-calcined MgO powder was then achieved by coating with stearic acid and ball milling [13].

Table 2 about here

Another advantage of calcining the MgO powder was a reduction of the particle size distribution; both the D10 and the D90 were significantly reduced compared to the uncalcined powder. The selected graphite pore former had an average particle size (d_{50} above 11 µm) a factor of ~7 larger than that of the calcined MgO powder (see Table 2) in order to introduce large stable pores in the microstructure to increase gas permeation in the support.

Fig. 2 shows a ternary compositional diagram for the thermoplastic feedstocks. The white area represents recipes that were able to be processed whereas the compositions in the grey regions could not be prepared due to problems with the kneading, warm pressing/extrusion or thermal treatment process.

Fig. 2 about here

For compositions with very high solids loading (MgO and graphite) of more than 65 vol.% the feedstock could not be homogenized due to incomplete wetting of the polymer and a very high viscosity (referred to as the “unmixable region”). At very high polymer contents above 65 vol.%, especially at high ratios of polymer to ceramic, the MgO structure deformed or collapsed during the shaping or heat treatment; this region is labeled “form instabilities”. In the region in the center of the ternary diagram (where the polymer and graphite content exceeded 65 vol.%) the prepared feedstocks were form-stable during extrusion but the MgO structures were not mechanically stable after sintering. Hence, only the white area of the compositional diagram, representing successful samples, was investigated in further detail. The data points in this region illustrate the three strategies for systematically studying the feedstock compositions (1) varying the polymer concentration (red data points, samples MP1-5), (2) increasing the pore former concentration with a fixed MgO content (blue data points, samples PG2-3) and (3) increasing the pore former concentration with a fixed polymer content (black data points, samples MG1-4).

3.2 Influence of polymer content on the porosity

Feedstocks with different ratios of polymer to ceramic were prepared to investigate the influence of the polymer content on the formation of open porosity after sintering. Table 3 summarizes the compositions and properties of warm-pressed planar structures before organic removal (green state), and after sintering.

Table 3 about here

As expected, the shrinkage and the porosity of the sintered MgO increased gradually from 15% to 21% and from 9% to 18%, respectively, with increasing polymer content (40% to 60%). It is clear that the porosity can be adjusted by simply changing the powder/polymer ratio, which is an advantage of using thermoplastic processing. However, even at the highest polymer content of 60 vol.% (the limit for producing a stable ceramic structure), the observed porosity of 18% is considered too low for sufficient gas permeability. Hence, the addition of a pore-former was required to create additional porosity. In Table 3 it can be seen that the packing density of the green warm-pressed samples increased gradually with increasing polymer content, clearly indicating that the flowability of the feedstocks increased. For MP1 with lowest polymer content of 40% the packing density of the green warm-pressed sample could be increased to values above 90% by further

optimization of the pressing parameters (temperature, pressure) but this was not the main purpose of this study.

3.3 Influence of pore former (50 vol.% ceramic)

In order to achieve high porosity values, the amount of pore former was gradually increased (replacing the polymer) at constant MgO powder concentration of 50 vol.%, as shown by the blue line in Fig. 2. Table 4 shows that the porosity could be significantly increased from 13% to 31% by the addition of 10% graphite in the MgO feedstock. It can be seen that feedstock PG3 (with 10% graphite) had a low packing density in the green state of 0.88. This indicates that (under the conditions used here for warm pressing), a polymer content of 40 vol.% is too low to achieve a homogeneous green body without small air inclusions. Hence, for this system, it can be concluded that the lower limit of the polymer content is above 40% in order to avoid air inclusions in the feedstock and subsequent processing problems.

Table 4 about here

3.4 Influence of pore former content on support properties (constant polymer content of 45 vol.%)

Table 5 shows the effect of graphite content (0 to 20 vol.%) on the properties of the sintered MgO (constant polymer content of 45 vol.%, sintered at 1275 °C). Comparing the compositions MP2, MG1 and MG2 with 0%, 5% and 10% graphite, respectively, the porosity increased almost linearly with the addition of graphite. It is worthwhile noting that the pore size distribution of the compositions changed from mono-modal to bi-modal at graphite concentrations above 10 vol.%. Furthermore, the size of the second peak representing the larger pore sizes increased with increasing pore former content.

Table 5 about here

Also shown in Table 5 are the data for MPG (19 vol.% graphite) which lie between those for MG3 and MG4 with respect to graphite content and final porosity. This composition was selected for further study as its porosity was within the targeted range (35-40%) and it showed the best overall behavior during processing (of the studied samples within the operational window shown in Fig. 2). Also, large quantities of MPG could be easily processed and hence this composition was considered suitable for up-scaling of the process in the future.

Fig. 3 shows SEM images of polished cross-sections of the MgO supports MP2 and MG1 to MG4. An increase in the absolute porosity and the fraction of larger pores was observed when the amount of pore former was increased from 0 to 20 vol.% (Fig. 3a to f). The graphite pore former produced the larger, elongated and oriented pores with sizes of several microns. The submicron porosity is from the removal of the polymer; these fine pores were also observed for composition MP2 (Fig. 3a), which contained no graphite.

Fig. 3 about here

3.4 Influence of sintering temperature

In the case where the MgO support will be co-sintered with a membrane layer, the densification behavior of the support during sintering must closely match that of the membrane to avoid mechanical failures e.g. cracking or delamination. Another challenge is to select a co-sintering temperature where the membrane can be fully densified while keeping sufficient porosity in the support. Hence, the densification behavior of the selected MgO feedstock (MPG) was investigated by dilatometry and compared to that of a CGO membrane sample (64 vol.% CGO and 36 vol.% polymer). The resulting densification curves in Fig. 4 show that more than 1300 °C is required for the membrane to reach a density above 85% (without an extended time at the sintering temperature). Further sintering experiments on CGO feedstocks showed that an isothermal holding time of about 2 h at 1300 °C achieved a density of 95% of theoretical density, which is considered to be sufficiently dense for the application. Hence, it was necessary to investigate the effect of higher sintering temperatures and the 2 h holding time on the porosity of the MgO. This was done by sintering warm-pressed samples of MPG at 1250 °C, 1300 °C, 1350 °C or 1400 °C for 2 h and analyzing the resulting porosity by SEM.

Fig. 4 about here

Fig. 5 shows the microstructures of the MgO samples sintered at different temperatures. At a sintering temperature of 1250 °C (Fig. 5a) large elongated pores from the graphite are visible (8.7 - 16.6 µm in length and aspect ratios between 1.5 and 4.8). When the sintering temperature was increased these larger pores grew slightly, whereas the MgO matrix (skeleton) densified as the finer pores from the polymer were eliminated (Fig. 5b).

Fig. 5 about here

Hg porosimetry measurements were performed on the same MgO samples as shown in Fig. 5 to quantify the development of the pore size distribution with sintering temperature. The pore size distributions of the MgO supports shown in Fig. 6 confirm the microstructural observations. For sintering temperatures of 1250 °C and 1300 °C bi-modal pore size distributions with two distinct peaks are observed; the first peak with an average size below 0.1 μm and the second peak including pores above 0.3 μm . This second peak is present for all four sintering temperatures. It is obvious that with increasing sintering temperature (from 1250 °C to 1350 °C) the smaller pores are completely eliminated from the MgO skeleton. As expected from the dilatometry measurements (Fig. 4), the porous MgO will sinter and densify at these temperatures and therefore the porosity below 0.1 μm will disappear. For the pores above 0.2 μm , the median pore diameter shifts from 0.3 to 0.7 when the final sintering temperature increased from 1250 °C to 1400 °C. The pore size distributions measured by Hg intrusion (Fig. 6) is significantly smaller compared to the microstructural observations (Fig. 5) and this discrepancy can be explained by the formation of bottleneck pores (e.g. submicron pores) which connect the larger (micrometer range) pores. In the Hg porosimetry technique the pore size is calculated from the pressure required to push the Hg through the sample and hence the bottleneck (smallest diameter of the pore) will give the measured pore size. Hence, the average pore size of samples with many bottleneck pores can be underestimated using this technique, which is why it was important also to view the microstructure.

The growth of the pores above 0.2 μm can be explained by the Oswald ripening process; the bottleneck pore size increased because of the densification of the MgO skeleton. The total porosity of the MgO samples as measured by Hg porosimetry is plotted as a function of sintering temperature in Fig. 6. As expected, the total porosity decreased with increasing sintering temperature until the sintering temperature reached 1350 °C. There was no further decrease in porosity observed at 1400 °C. The strong decrease in porosity in the temperature range 1250-1350 °C was a result of the elimination of the small pores in the MgO skeleton (as evidenced by the disappearance of the smaller pore size peak in Fig. 6).

Fig. 6 about here

3.5 Permeability of the MgO supports

Gas permeation measurements for the MPG samples were conducted in order to correlate the gas flow through the porous structure with the microstructure developed at different sintering temperatures. The permeability of the supports at ΔP of 200 kPa is plotted (left axis) as a function of the sintering temperature in Fig. 7a, along with the porosity of the supports (right axis).

Fig. 7 a, b about here

The permeability was highest for the sample sintered at the lowest temperature of 1250 °C (with the bi-modal pore size distribution as shown in Fig. 6) and decreased by a factor of more than 3 for a sintering temperature of 1300 °C. Increasing the sintering temperature further to 1350 °C and 1400 °C did not further decrease the permeability as could be expected from the lower total porosity values. In fact the permeability of the sample sintered at 1400 °C was a factor of 2.5 larger than that of the sample sintered at 1350 °C. Considering the microstructural development discussed in the previous section, it is clear that the gas permeation depends not only on the total porosity, but also on the microstructure (pore size, pore shape and interconnectivity of the pores or “tortuosity”). Fig. 7b shows a significant increase in the volume fraction of the larger pores (above 0.5 μm) from below 20% to almost 90% when the sintering temperature was increased from 1300 to 1350 °C. Furthermore, the median pore size is more than doubled over the same range. Despite a reduction in the total porosity with increasing temperature, it is clear that the microstructures developed at higher sintering temperatures are beneficial for gas permeation (a higher fraction of large interconnected pores). This is a positive result with respect to co-sintering the MgO supports with CGO membranes; the evaluated sintering temperatures (above 1300 °C) required for densifying the CGO are not detrimental for gas permeability and are likely to be beneficial for the mechanical strength of the porous supports.

4. Conclusion

Magnesium oxide has a relatively high thermal expansion coefficient compared to other structural ceramics, which makes it a suitable, generic support material for OTM materials such as perovskites or ceria-based materials. Supports with a high total porosity (up to 36%) and an average pore size $\sim 0.5 \mu\text{m}$ were

achieved using a feedstock with 19 vol.% graphite pore former (particle size $\sim 10\ \mu\text{m}$) and a sintering temperature of $1300\ ^\circ\text{C}$. A significant, unexpected increase in gas permeation through the porous MgO supports was observed when the sintering temperature was increased from 1300 to $1400\ ^\circ\text{C}$, despite a significant decrease in the total porosity. This was explained by the growth and homogenization of the larger pores introduced by the pore former and by improved interconnectivity of the pores (broadening of the pore channels) due to densification. The optimization of the MgO feedstock resulted in porous supports with suitable microstructures and sintering activity for co-sintering with CGO at temperatures between $1300\ ^\circ\text{C}$ and $1400\ ^\circ\text{C}$. In the case where these MgO supports would be used with high-performance membrane layers (delivering oxygen fluxes of $10\ \text{ml min}^{-1}\ \text{cm}^{-2}$ or more), these gas permeabilities of 1.4 to $3.1 \times 10^{-16}\ \text{m}^2$ may limit the performance of the membrane. Therefore further research is being undertaken to enlarge the average pore size of the MgO supports using alternative pore formers while optimizing the mechanical strength (e.g. using spherical graphite to form more homogenous pores). In addition, extrusion of these thermoplastic feedstocks is being undertaken to produce thin-walled porous MgO tubes onto which catalytic layers and ceria-based membrane layers can be applied by dip-coating and then co-sintered to produce fully functional OTMs.

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6. References

- [1] M. Salehi, F. Clemens, E.M. Pfaff, S. Diethelm, C. Leach, T. Graule, et al., A case study of the effect of grain size on the oxygen permeation flux of BSCF disk-shaped membrane fabricated by thermoplastic processing, *J. Memb. Sci.* 382 (2011) 186–193.
- [2] X. Zhu, S. Sun, Y. Cong, W. Yang, Operation of perovskite membrane under vacuum and elevated pressures for high-purity oxygen production, *J. Memb. Sci.* 345 (2009) 47–52.

- [3] C. Delbos, G. Lebain, N. Richet, C. Bertail, Performances of tubular $\text{La}_{0.8}\text{Sr}_{0.2}\text{Fe}_{0.7}\text{Ga}_{0.3}\text{O}_{3-\delta}$ mixed conducting membrane reactor for under pressure methane conversion to syngas, *Catal. Today*. 156 (2010) 146–152.
- [4] P.V. Hendriksen, P.H. Larsen, M. Mogensen, F.W. Poulsen, K. Wiik, Prospects and problems of dense oxygen permeable membranes, *Catal. Today*. 56 (2000) 283–295.
- [5] J. Sunarso, S. Baumann, J.M. Serra, W.A. Meulenbergh, S. Liu, Y.S. Lin, et al., Mixed ionic-electronic conducting (MIEC) ceramic-based membranes for oxygen separation, *J. Memb. Sci.* 320 (2008) 13–41.
- [6] a. Kaiser, S. Foghmoes, C. Chatzichristodoulou, M. Søggaard, J. a. Glasscock, H.L. Frandsen, et al., Evaluation of thin film ceria membranes for syngas membrane reactors—Preparation, characterization and testing, *J. Memb. Sci.* 378 (2011) 51–60.
- [7] C. Chatzichristodoulou, M. Søggaard, J. Glasscock, A. Kaiser, S.P.V. Foghmoes, P.V. Hendriksen, Oxygen Permeation in Thin, Dense $\text{Ce}_{0.9}\text{Gd}_{0.1}\text{O}_{1.95-\delta}$ Membranes II. Experimental Determination, *J. Electrochem. Soc.* 158 (2011) F73.
- [8] C. Zhang, Z. Xu, X. Chang, Z. Zhang, W. Jin, Preparation and characterization of mixed-conducting thin tubular membrane, *J. Memb. Sci.* 299 (2007) 261–267.
- [9] D. Bayraktar, F. Clemens, S. Diethelm, T. Graule, J. Van Herle, P. Holtappels, Production and properties of substituted LaFeO_3 -perovskite tubular membranes for partial oxidation of methane to syngas, *J. Eur. Ceram. Soc.* 27 (2007) 2455–2461.
- [10] a. Chanda, B.X. Huang, J. Malzbender, R.W. Steinbrech, Micro- and macro-indentation behaviour of $\text{Ba}_{0.5}\text{Sr}_{0.5}\text{Co}_{0.8}\text{Fe}_{0.2}\text{O}_{3-\delta}$ perovskite, *J. Eur. Ceram. Soc.* 31 (2011) 401–408.
- [11] D.C. Zhu, X.Y. Xu, S.J. Feng, W. Liu, C.S. Chen, La_2NiO_4 tubular membrane reactor for conversion of methane to syngas, *Catal. Today*. 82 (2003) 151–156.
- [12] R.Z. Liu, S.R. Wang, B. Huang, C.H. Zhao, J.L. Li, Z.R. Wang, et al., Dip-coating and co-sintering technologies for fabricating tubular solid oxide fuel cells, *J. Solid State Electrochem.* 13 (2008) 1905–1911.
- [13] M. Salehi, E.M. Pfaff, R.M. Junior, C.P. Bergmann, S. Diethelm, C. Neururer, et al., $\text{Ba}_{0.5}\text{Sr}_{0.5}\text{Co}_{0.8}\text{Fe}_{0.2}\text{O}_{3-\delta}$ (BSCF) feedstock development and optimization for thermoplastic forming of thin planar and tubular oxygen separation membranes, *J. Memb. Sci.* 443 (2013) 237–245.
- [14] F. Clemens, Thermoplastic Extrusion for Ceramic Bodies, in: F. Händle (Ed.), *Extrus. Ceram.*, Springer Verlag Heidelberg, 2007: pp. 323–345.
- [15] M. Lipińska-Chwałek, G. Pećanac, J. Malzbender, Creep behaviour of membrane and substrate materials for oxygen separation units, *J. Eur. Ceram. Soc.* 33 (2013) 1841–1848.
- [16] K. Kwok, H.L. Frandsen, M. Søggaard, P.V. Hendriksen, Stress analysis and fail-safe design of bilayered tubular supported ceramic membranes, *J. Memb. Sci.* 453 (2014) 253–262.
- [17] Y. Shiratori, YSZ–MgO composite electrolyte with adjusted thermal expansion coefficient to other SOFC components, *Solid State Ionics*. 164 (2003) 27–33.
- [18] F. Jtilich, D.- Jtilich, Thermal Expansion of SOFC Materials, 5 (1999) 129–139.

- [19] J. Heiber, F. Clemens, T. Graule, D. Hülseberg, Thermoplastic Extrusion to Highly-Loaded Thin Green Fibres Containing $\text{Pb}(\text{Zr,Ti})\text{O}_3$, *Adv. Eng. Mater.* 7 (2005) 404–408.
- [20] M. Trunec, J. Cihlar, Thermal removal of multicomponent binder from ceramic injection mouldings, *J. Eur. Ceram. Soc.* 22 (2002) 2231–2241.
- [21] J. Heiber, F. Clemens, T. Graule, D. Hülseberg, Influence of Fibre Diameter on the Microstructure and the Piezoelectric Properties of PZT-Fibres, *Adv. Sci. Technol.* 45 (2006) 2459–2463.

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Fig. 3 : SEM micrographs of MgO supports with various graphite contents a) no graphite (MP2), b) 5% graphite (MG1), c) 10% graphite (MG2), d) 15% graphite (MG3), e) 20% graphite (MG4), f) 19% graphite (MPG). The samples were sintered at 1275 °C for 2 h.

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Table 1. Feedstocks: (MP1-MP5) with various ceramic to polymer ratios and no pore former; (PG2-3) two different pore former contents with a constant ceramic concentration of 50 vol.%; (MG1-4) different pore former contents with a constant polymer content of 45 vol.%; and (MPG) final feedstock composition that was optimized for up-scaling.

Code	MgO content Vol.%	Polymer & additives Vol.%	Graphite Vol.%
Various ceramic contents (no pore former)			
MP1	60	40	-
MP2	55	45	-
MP3	50	50	-
MP4	45	55	-
MP5	40	60	-
Various pore former contents, constant MgO content 50 vol.%			
MP3	50	50	0
PG2	50	45	5
PG3	50	40	10
Various pore former contents, constant polymer content 45 vol.%			
MG1	50	45	5
MG2	45	45	10
MG3	40	45	15
MG4	35	45	20
Optimized feedstock composition			
MPG	39	42	19

Table 2. BET specific surface area, particle-size distribution (PSD), and the calculated agglomeration factor (AF) for MgO powder (uncalcined and calcined at 1000 °C) and graphite powder.

Powder	Specific surface area (m ² /g)	*PSD (μm)			Agglomeration factor (AF)
		D10	D50	D90	
MgO, uncalcined	78.0	0.510	2.99	40.8	140.0
MgO, 1000°C, 10 h	10.8	0.187	1.53	6.07	10.0
Graphite	10.5	6.53	11.3	19.9	----

* PSD measured by laser diffraction after ball milling in ethanol for 24 h (see section 2.1).

Table 3. Properties of MgO support layers with different polymer contents after sintering at 1275 °C for 2 h (* measured by Hg porosimetry).

Composition		Green state		Sintered state		
Code	Polymer	Density (g/cm ³)	Packing density ^a	Linear Shrinkage (%)	*Porosity (%)	Pore size (μm)
MP1	40	2.22	0.88 ± 0.02	15.1	9.2	0.10
MP2	45	2.20	0.92 ± 0.02	15.7	13.5	0.07
MP3	50	2.12	0.94 ± 0.02	15.9	13.0	0.11
MP4	55	1.98	0.94 ± 0.02	17.9	13.5	0.12
MP5	60	1.90	0.96 ± 0.02	20.8	18.2	0.15

^a Packing density at green state is defined here as the geometrical green density (column 3) compared to the expected green density calculated from the densities and concentrations of each component.

Table 4. Porosity and shrinkage of MgO supports sintered at 1275 °C for 2 h (constant ceramic content of 50 vol.%) as a function of the graphite to polymer ratio.

Composition			Green state		Sintered state		
Code	Polymer	Graphite	Density (g/cm ³)	Packing density	Linear Shrinkage (%)	Porosity (%)	Pore size (μm)
MP3	50	0	2.12	0.94 ± 0.02	15.9	13.0	0.11
PG2	45	5	2.20	0.96 ± 0.02	15.1	17.1	0.14
PG3	40	10	2.08	0.88 ± 0.02	15.3	30.9	0.26

Table 5. Porosity and shrinkage of MgO supports sintered at 1275 °C for 2 h (constant polymer content of 45 vol.%) as a function of the graphite to MgO ratio.

Composition				Green state		Sintered state			
Code	Ceramic	Polymer	Graphite	Density (g/cm ³)	Packing density	Shrinkage (%)	Porosity (%)	Pore size peaks* (μm)	
								P1	P2
MP2	55	45	0	2.19	0.92 ±0.02	15.7	14.4	0.10	---
MG1	50	45	5	2.21	0.94 ±0.02	15.1	16.0	0.15	---
MG2	45	45	10	2.20	0.98 ±0.02	15.2	19.4	0.20	---
MG3	40	45	15	2.18	0.96 ±0.02	14.9	32.5	0.21	0.36
MG4	35	45	20	2.03	0.96 ±0.02	12.1	47.5	0.08	0.42
MPG	39	42	19	2.08	0.94 ±0.02	13.42	37.0	0.06	0.40

*Bi-model pore size distribution (peaks labelled P1 and P2) was observed only when the graphite concentration was more than 10%.

